

WP3.1.4: *FEA of TMC ATLLAS generic leading edge model wing*

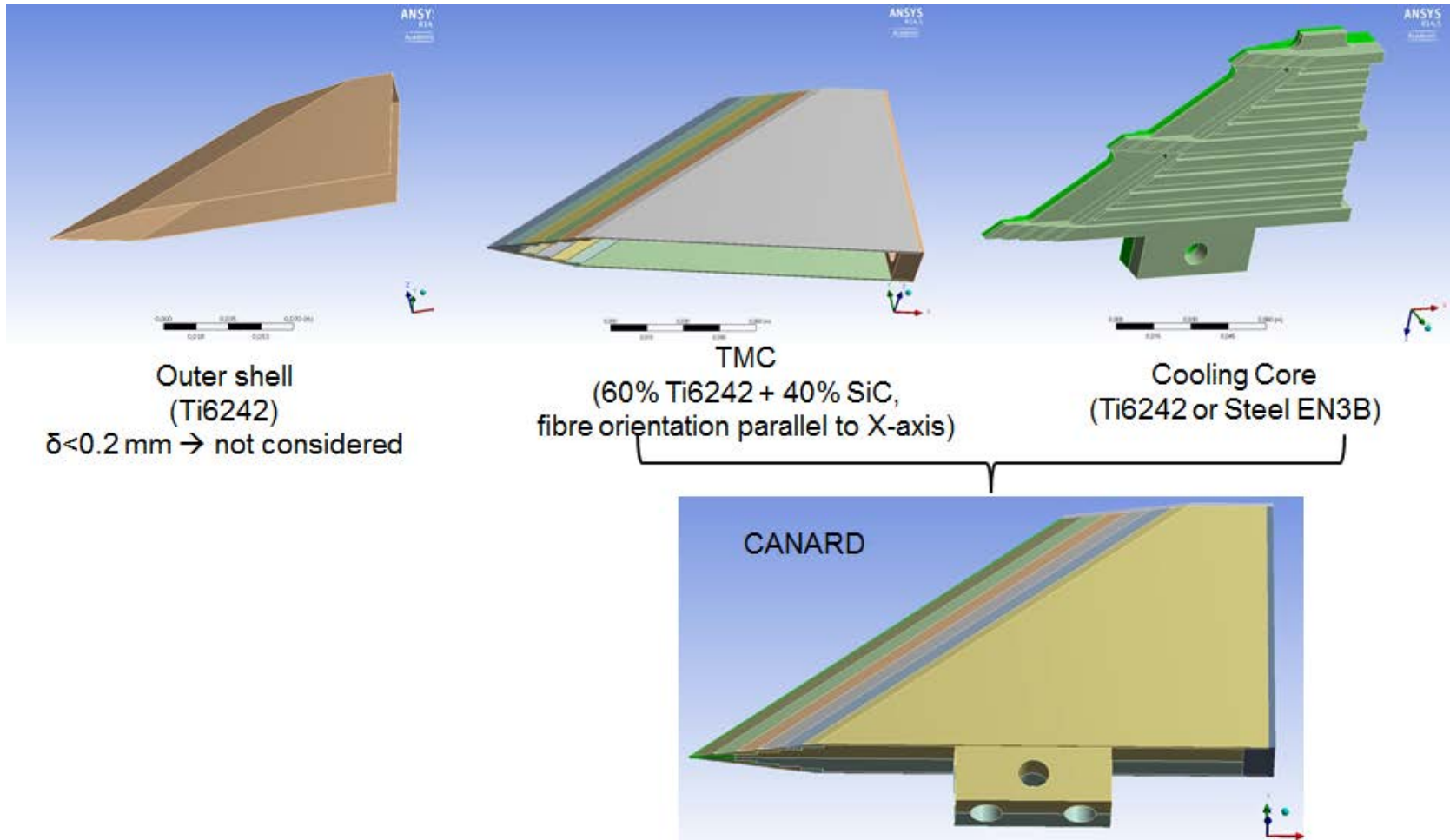
Numerical modelling of TMC ATLLAS generic leading edge model wing: discovered problems and technical solutions

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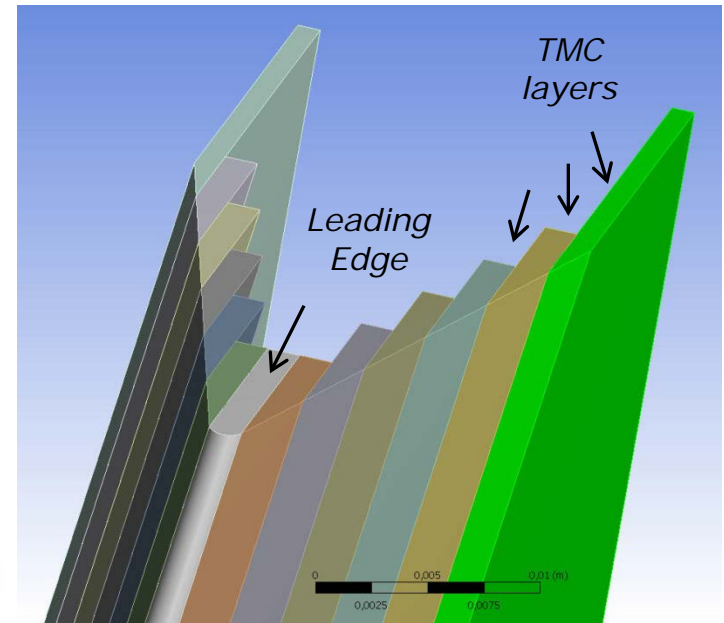
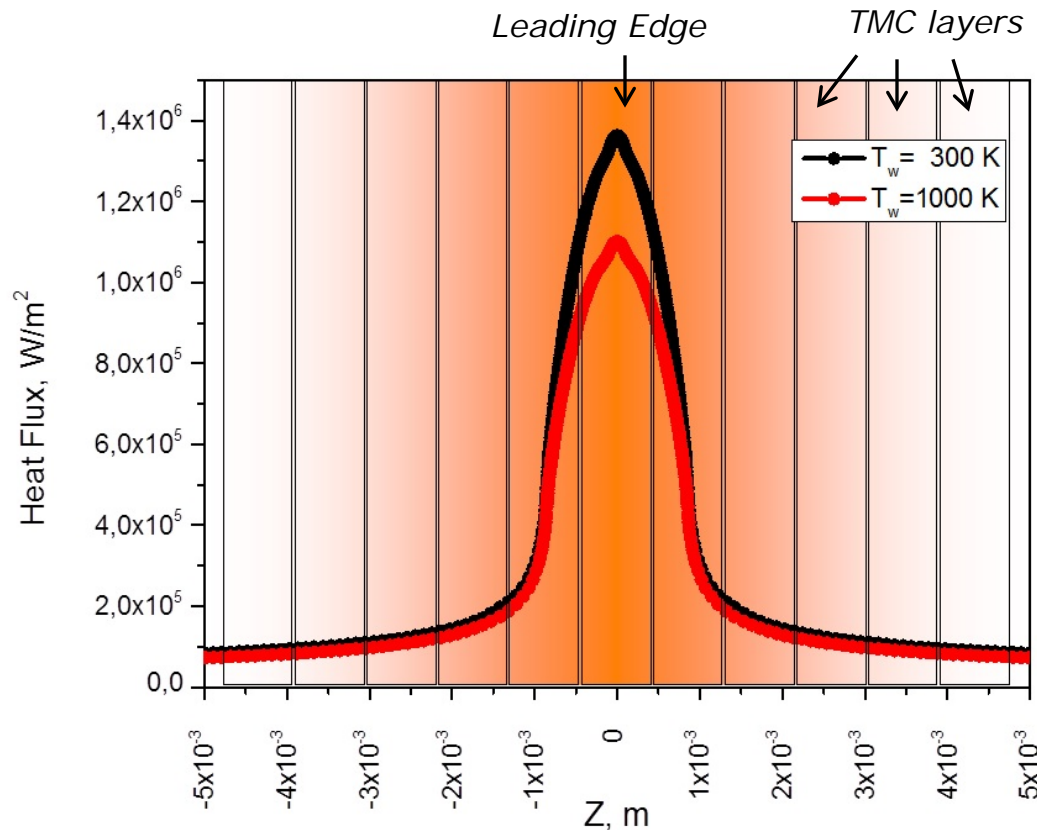
CANARD Model

- FEA of TMC ATLLAS generic leading edge model wing – CANARD is designed and provided by TISICS (calculation using **ANSYS®**)



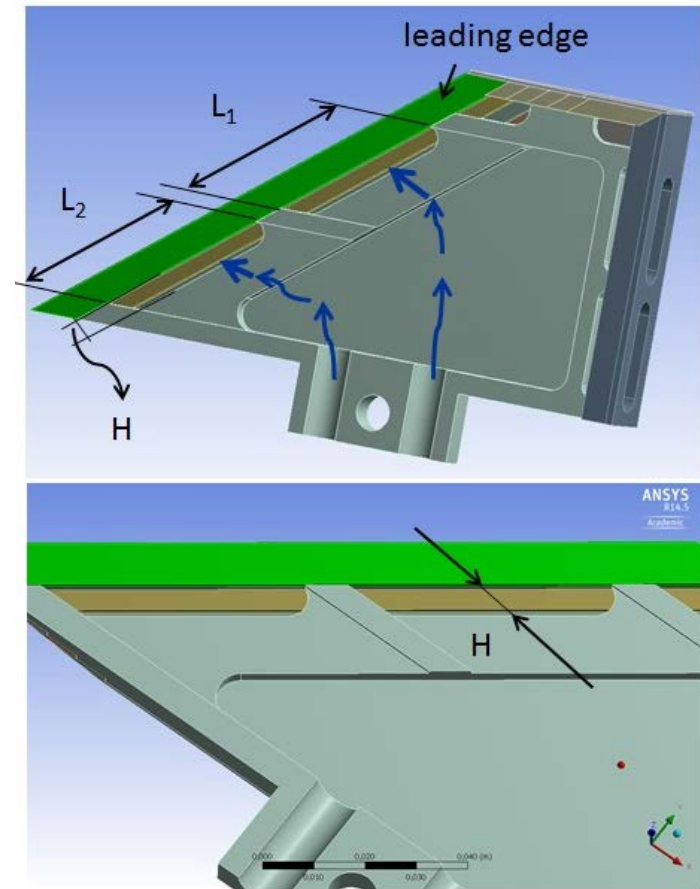
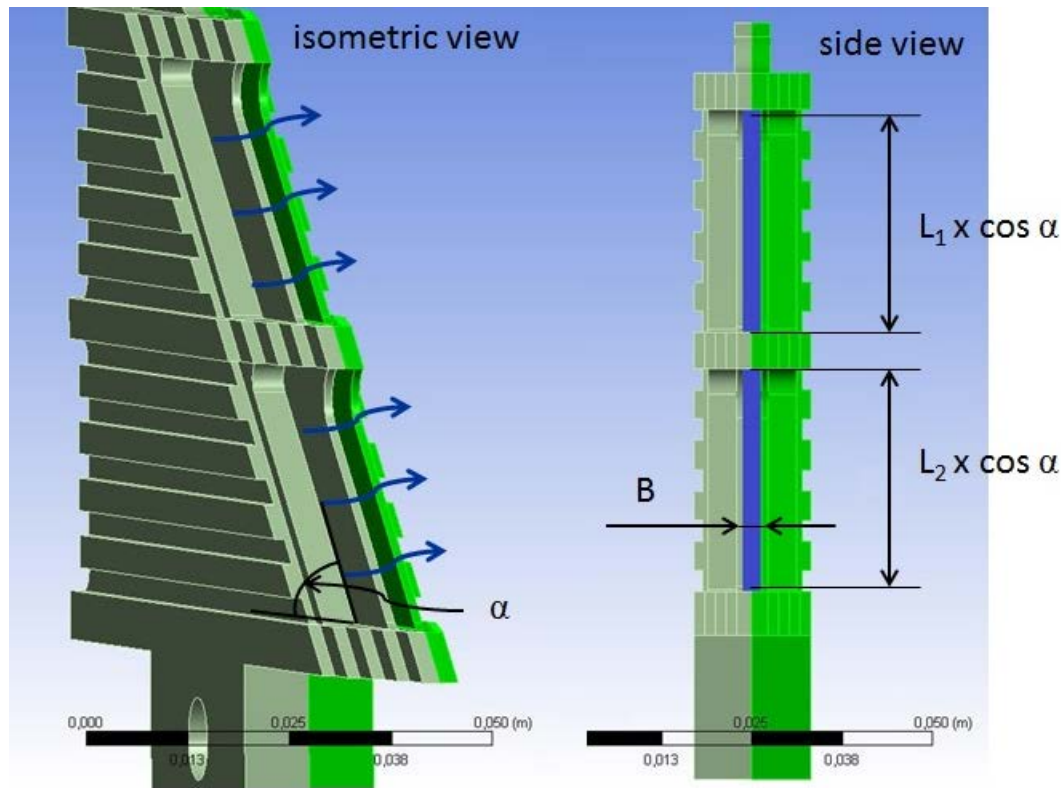
Heating

Heat flux distribution over the TMC layers



Testing in L3K DLR's arc heated facility: calculation by Dr. B. Esser (DLR) for the radiused leading edge of $0,8 \text{ mm}$ for the two constant wall temperatures of 300 K and 1000 K

Back Impingement Cooling of leading TMC part

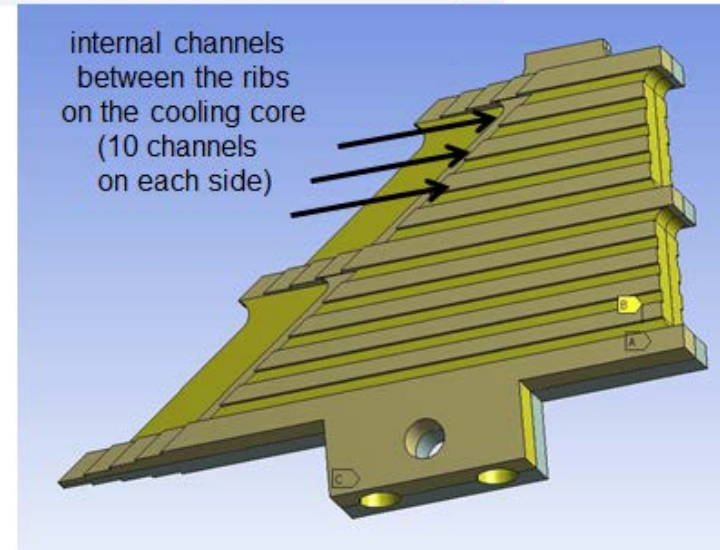
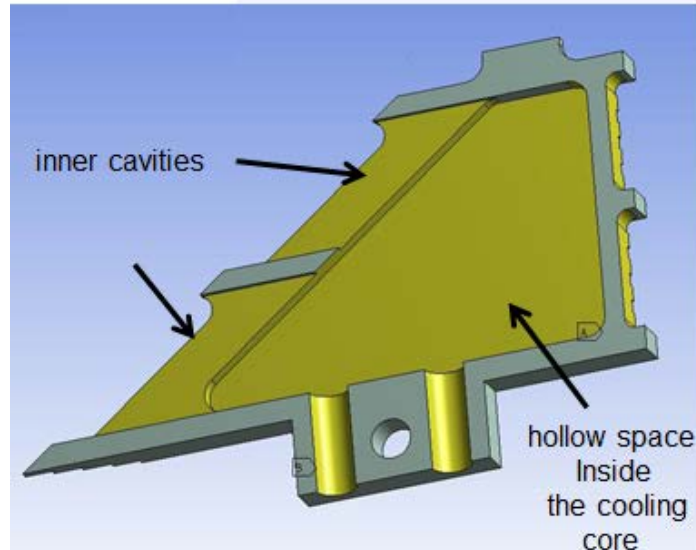
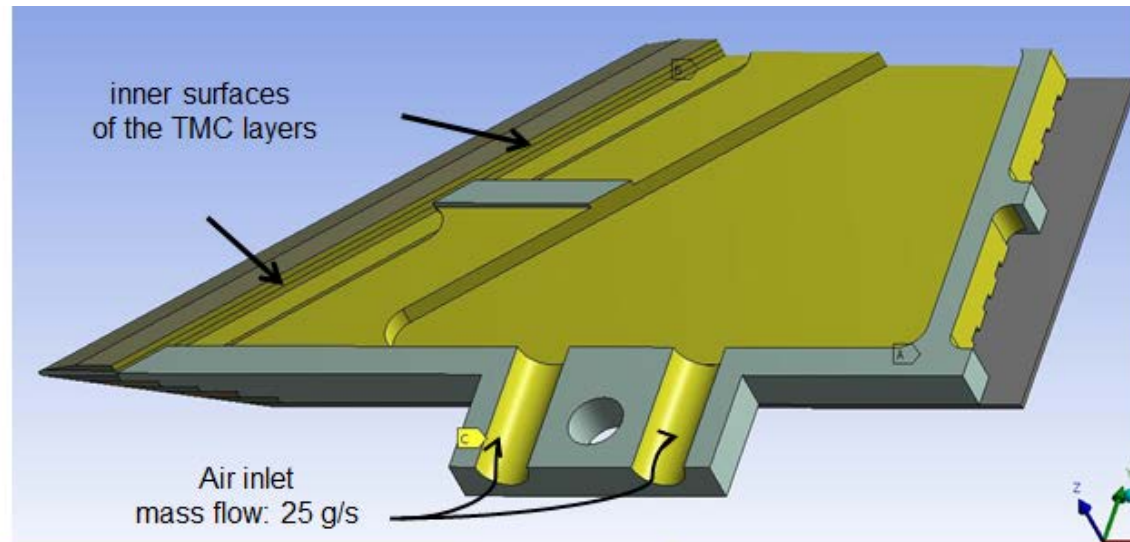


Slot jet (blue area) with the following geometric parameters:

$B = 5 \text{ mm}$ – width of slots;

$L_1 = L_2 = 50 \text{ mm}$ - length of slots

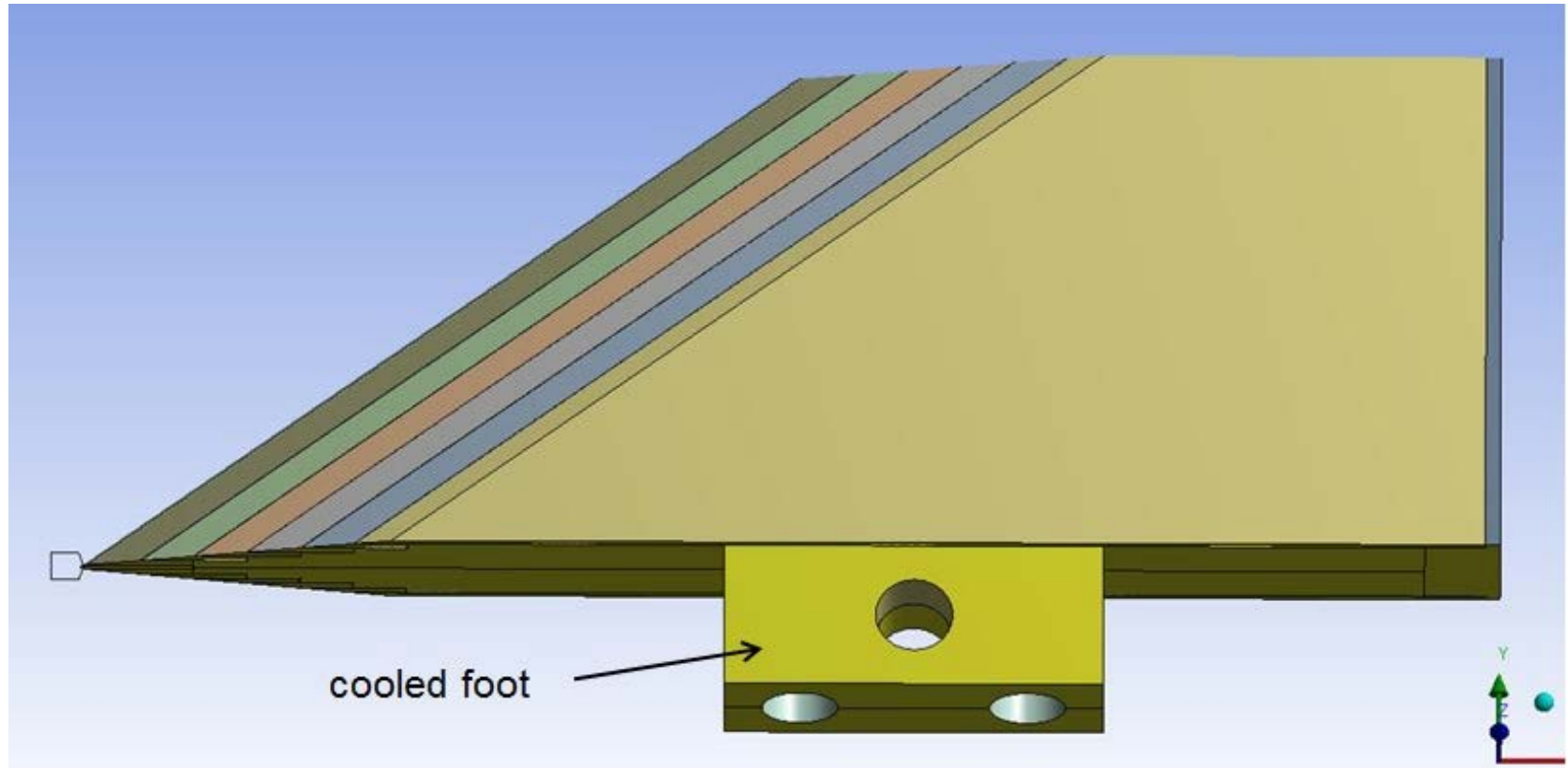
Internal Air Cooling (forced convection)



Cooled surfaces are marked in yellow

Heat transfer coefficients calculation - s. in Annex 2

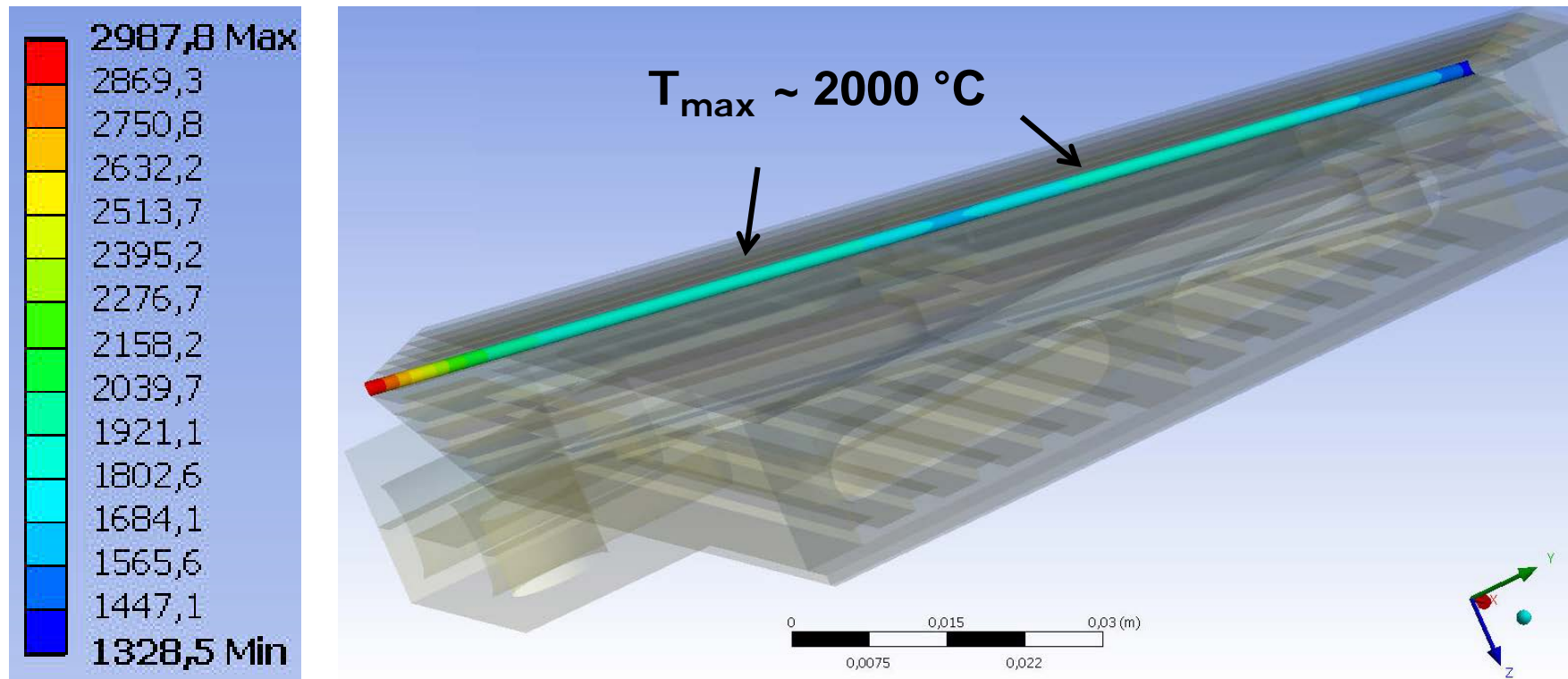
Water cooling on the lower part



CANARD Model (I): High Temperature Level

Leading edge temperature

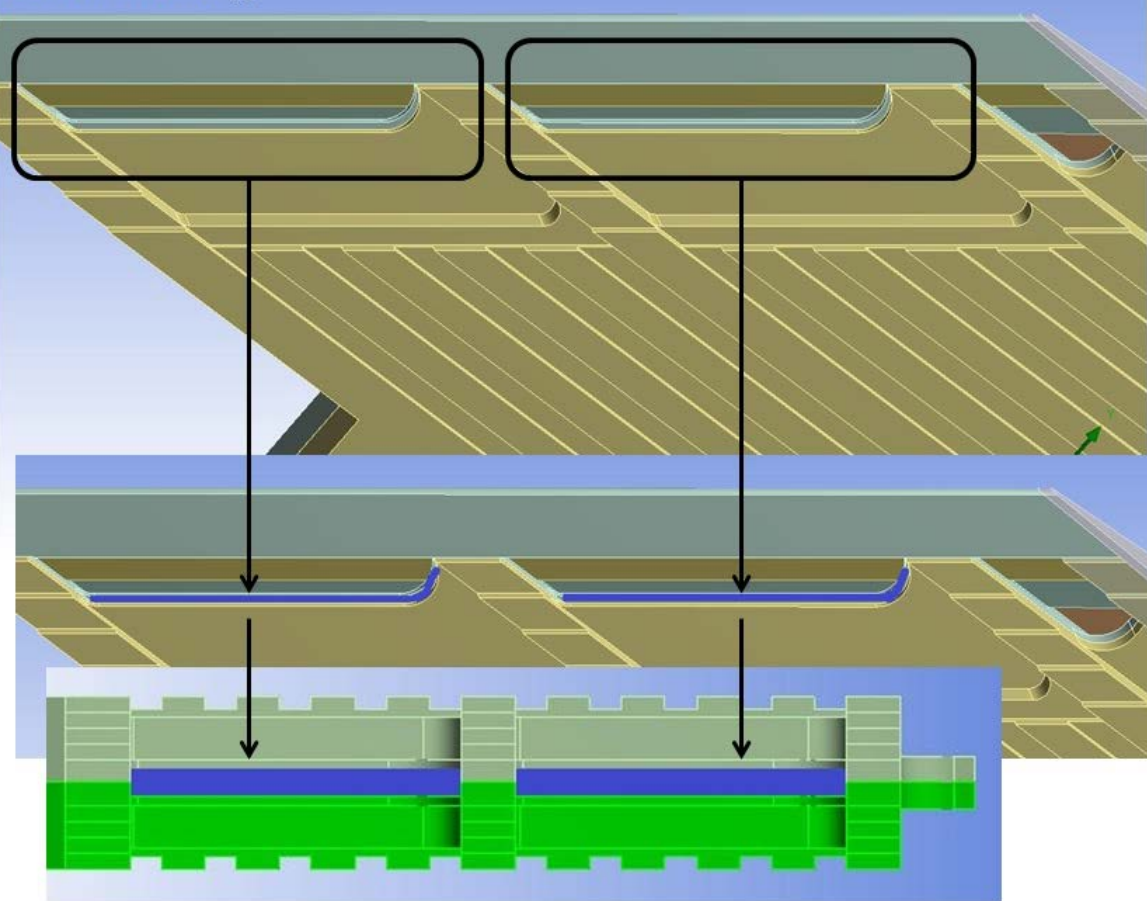
- air mass flow: 25 g/s
- maximum heat flow: $1.02 \times 10^6 \text{ W/m}^2$
- cooling core: steel EN3B



Note: Operational limits of TMC's material exceed significantly

CANARD Model (I) does not provide adequate cooling

CANARD Model (I)

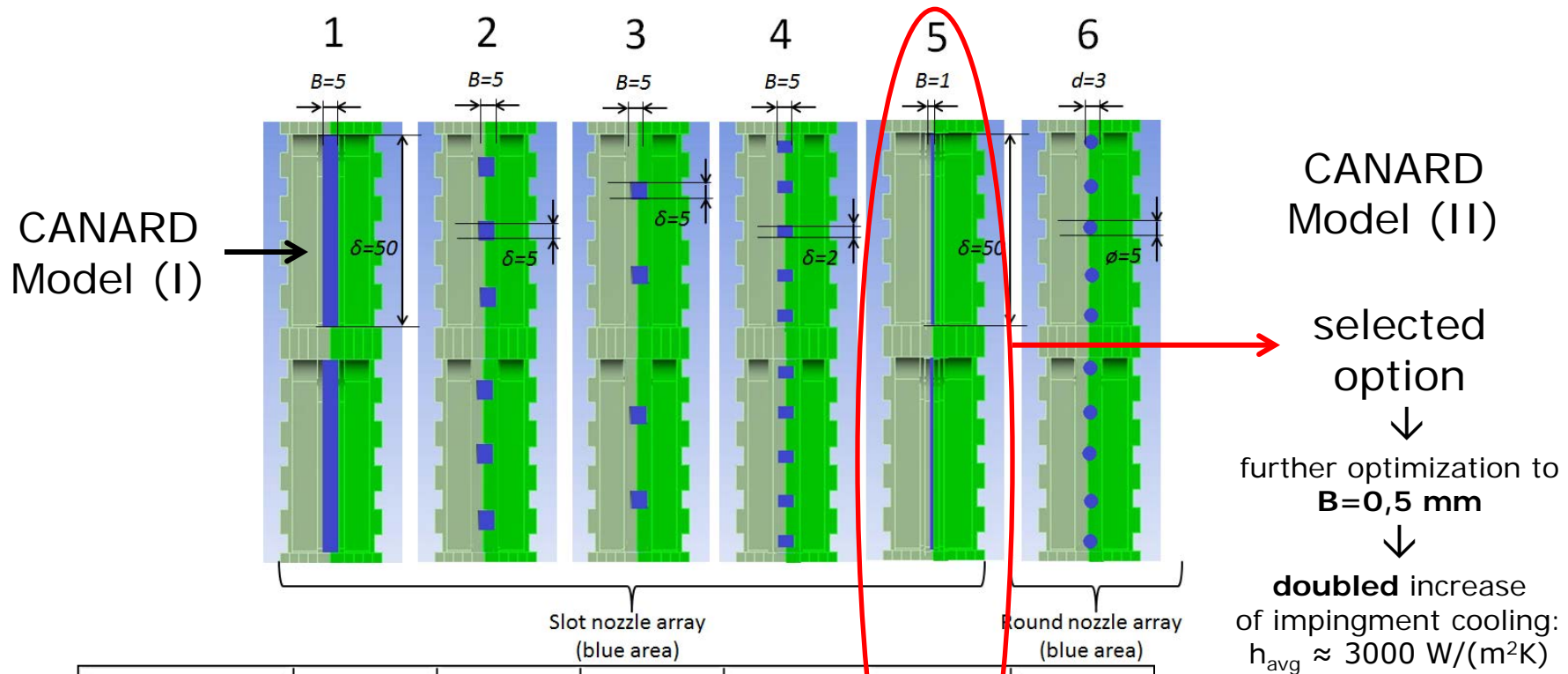


The occurring slot velocities for impingement cooling were detected to be too low which effects in low heat transfer coefficients and hence cooling efficiency

The size of the cooling slots (blue areas) and mainly its width must be significantly reduced in terms of increasing the air flow rate

CANARD Models (II): reduced cooling slots

Variations of slit nozzle:

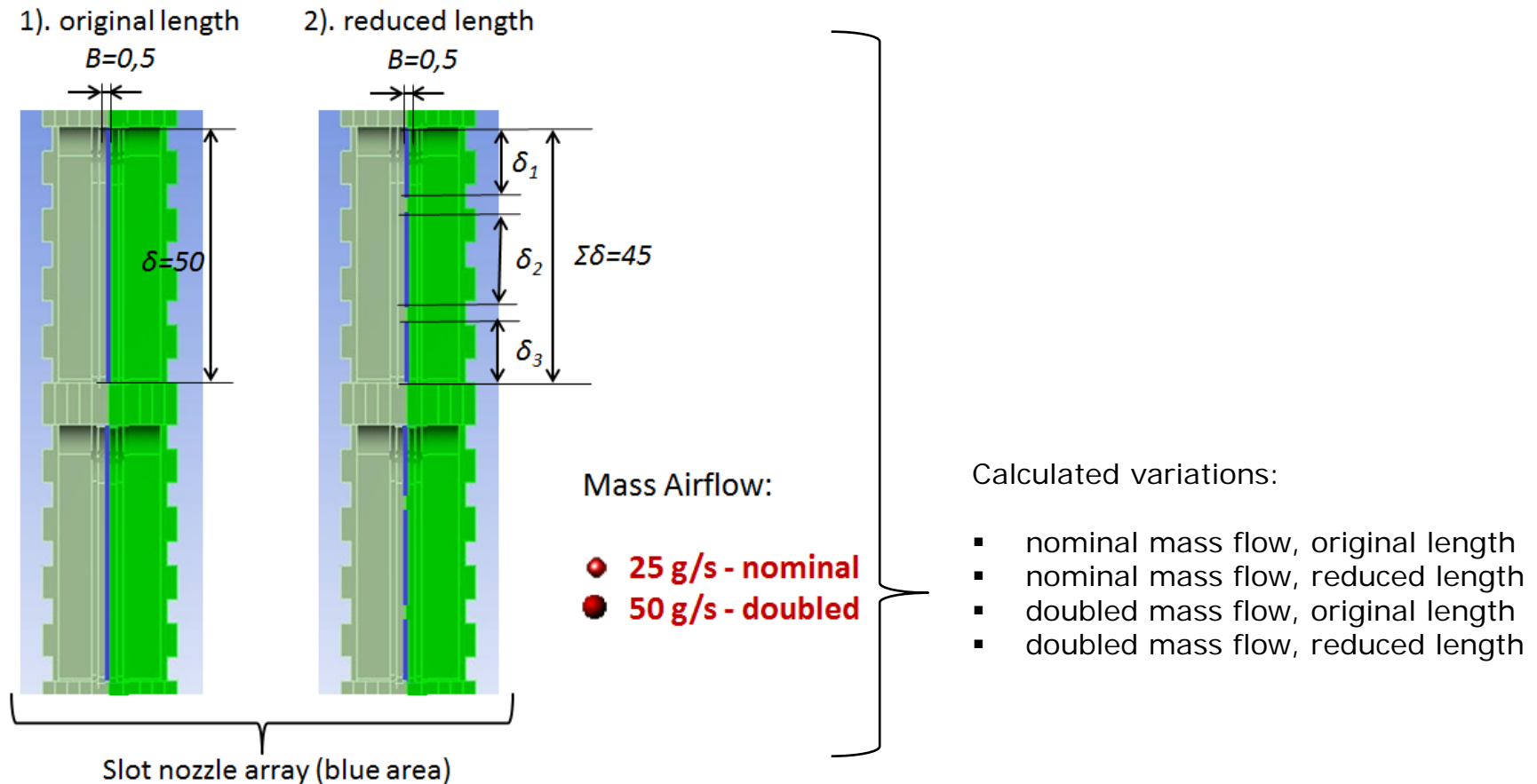


impingement	1	2	3	4	5	6
$h_{\text{avg}}, \text{W/(m}^2\text{K)}$	148	783	1053	1500	1525	1120

10 times increased

CANARD Models (II): further optimization

Thin slit nozzle with $B=0,5$ mm



Impingement heat transfer coefficients in CANARD Models (II):

Nominal Mass Airflow: ● 25 g/s (P = 1 bar, T = 20 °C)		Doubled Mass Airflow: ● 50 g/s (P = 4 bar, T = 20 °C)	
Original length	Reduced length	Original length	Reduced length
B = 0,5 mm $\delta = 50 \text{ mm}$ $L = 2 \times \delta =$ $= 2 \times 50 =$ $= 100 \text{ mm}$ $S = B \times L = 50 \text{ mm}^2$ Defining parameter: B H = 6 mm Martin [1]: for array of slot nozzle $h_{\text{avg}} = 2800 \text{ W}/(\text{m}^2\text{K})$	B = 0,5 mm $\Sigma\delta = 45 \text{ mm}$ $L = 2 \times \Sigma\delta =$ $= 2 \times 45 =$ $= 90 \text{ mm}$ $S = B \times L = 45 \text{ mm}^2$ Defining parameter: B H = 6 mm Martin [1]: for array of slot nozzle $h_{\text{avg}} = 3000 \text{ W}/(\text{m}^2\text{K})$	B = 0,5 mm $\delta = 50 \text{ mm}$ $L = 2 \times \delta =$ $= 2 \times 50 =$ $= 100 \text{ mm}$ $S = B \times L = 50 \text{ mm}^2$ Defining parameter: B H = 6 mm Martin [1]: for array of slot nozzle $h_{\text{avg}} = 4455 \text{ W}/(\text{m}^2\text{K})$	B = 0,5 mm $\Sigma\delta = 45 \text{ mm}$ $L = 2 \times \Sigma\delta =$ $= 2 \times 45 =$ $= 90 \text{ mm}$ $S = B \times L = 45 \text{ mm}^2$ Defining parameter: B H = 6 mm Martin [1]: for array of slot nozzle $h_{\text{avg}} = 4780 \text{ W}/(\text{m}^2\text{K})$

Main heat transfer coefficients in *CANARD Models (II)*:

Nominal Mass Airflow: ● 25 g/s (P = 1 bar, T = 20 °C)		Doubled Mass Airflow: ● 50 g/s (P = 4 bar, T = 20 °C)	
Original length	Reduced length	Original length	Reduced length
Impingement: $h_{avg} = 2800 \text{ W/(m}^2\text{K)}$	Impingement: $h_{avg} = 3000 \text{ W/(m}^2\text{K)}$	Impingement: $h_{avg} = 4455 \text{ W/(m}^2\text{K)}$	Impingement: $h_{avg} = 4780 \text{ W/(m}^2\text{K)}$
Input: $h_{avg} = 500 \text{ W/(m}^2\text{K)}$	Input: $h_{avg} = 500 \text{ W/(m}^2\text{K)}$	Input: $h_{avg} = 900 \text{ W/(m}^2\text{K)}$	Input: $h_{avg} = 900 \text{ W/(m}^2\text{K)}$
Inner surfaces: $230 < h_{avg} < 1000$	Inner surfaces: $230 < h_{avg} < 1000$	Inner surfaces: $410 < h_{avg} < 1800$	Inner surfaces: $410 < h_{avg} < 1800$
Side ribs: $h_{avg} = 1000 \text{ W/(m}^2\text{K)}$	Side ribs: $h_{avg} = 1000 \text{ W/(m}^2\text{K)}$	Side ribs: $h_{avg} = 1800 \text{ W/(m}^2\text{K)}$	Side ribs: $h_{avg} = 1800 \text{ W/(m}^2\text{K)}$
Water cooling (bottom): $h_{avg} = 8000 \text{ W/(m}^2\text{K)}$	Water cooling (bottom): $h_{avg} = 8000 \text{ W/(m}^2\text{K)}$	Water cooling (bottom): $h_{avg} = 8000 \text{ W/(m}^2\text{K)}$	Water cooling (bottom): $h_{avg} = 8000 \text{ W/(m}^2\text{K)}$
Back outer part: $h_{avg} = 20 \text{ W/(m}^2\text{K)}$	Back outer part: $h_{avg} = 20 \text{ W/(m}^2\text{K)}$	Back outer part: $h_{avg} = 20 \text{ W/(m}^2\text{K)}$	Back outer part: $h_{avg} = 20 \text{ W/(m}^2\text{K)}$

Heating of the front TMC strips

N	Z, m	Heat Flux, W/m ²		h, W/(m ² K)		T, K		T, °C	Surfaces
		max	average	max	average	max	average	average	
1	0,0E+00	1100608,1	1024472,8	374,1	336,0	3942	4063	3790	front edge of TMC part 1 central leading edge
2	4,0E-04	948337,5	576606,9	297,8	164,5	4184	5869	5596	front edge of TMC part 2
3	1,2E-03	204876,2	166012,7	31,3	26,8	7554	7129	6855	front edge of TMC part 3
4	2,0E-03	127149,2	114901,6	22,3	21,2	6703	6396	6123	front edge of TMC part 4
5	2,8E-03	102653,9	95010,5	20,2	19,0	6089	5992	5719	front edge of TMC part 5
6	3,6E-03	87367,1	82269,3	17,8	17,5	5895	5698	5425	front edge of TMC part 6
7	4,4E-03	77171,5	74834,8	17,1	16,5	5502	5527	5254	front edge of TMC part 7
8	5,2E-03	72498,1	38585,7	15,9	15,9	5552	5552	5279	8 - side panel of TMC part 7, parallel to the heat flow

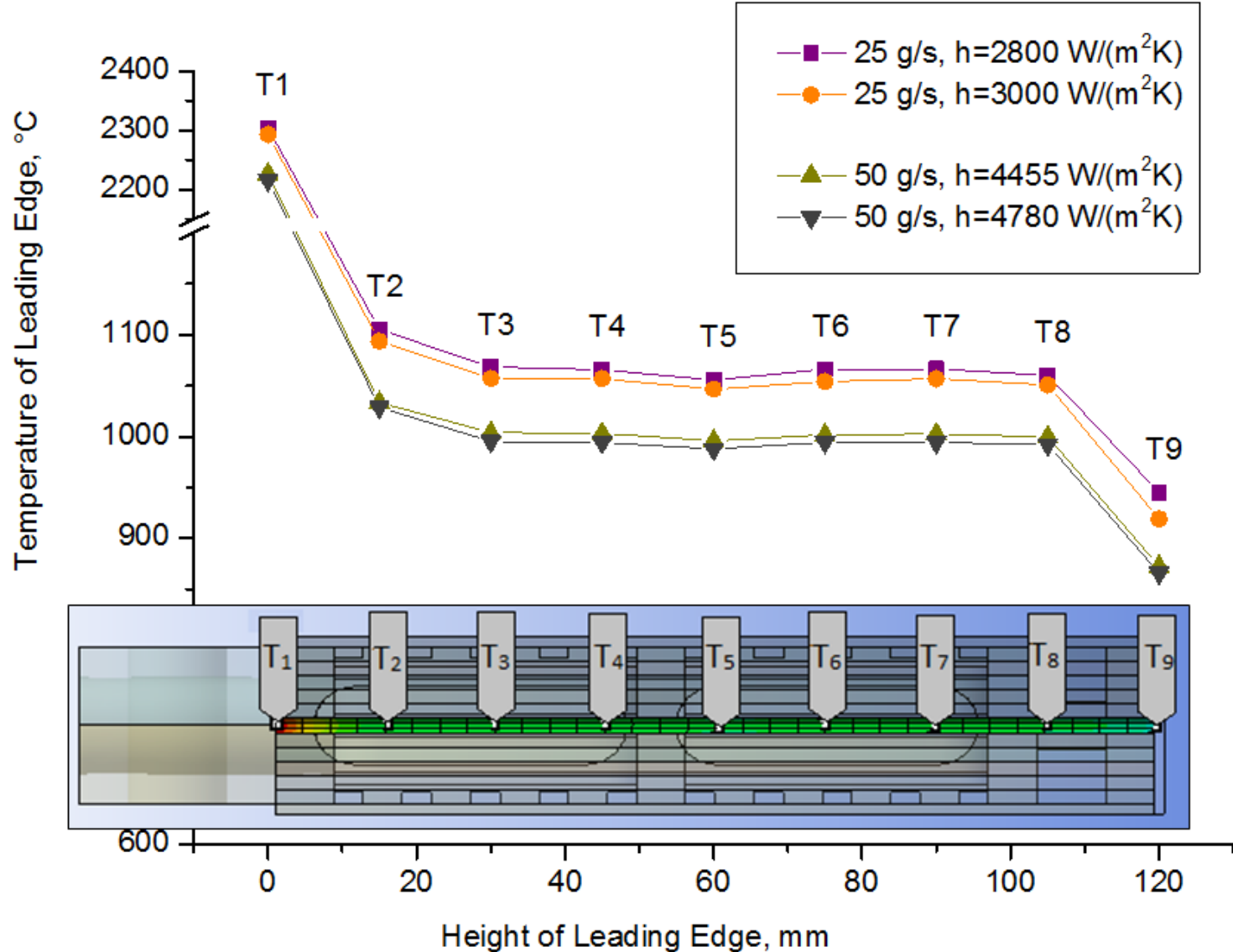
Used in calculation as convective flow



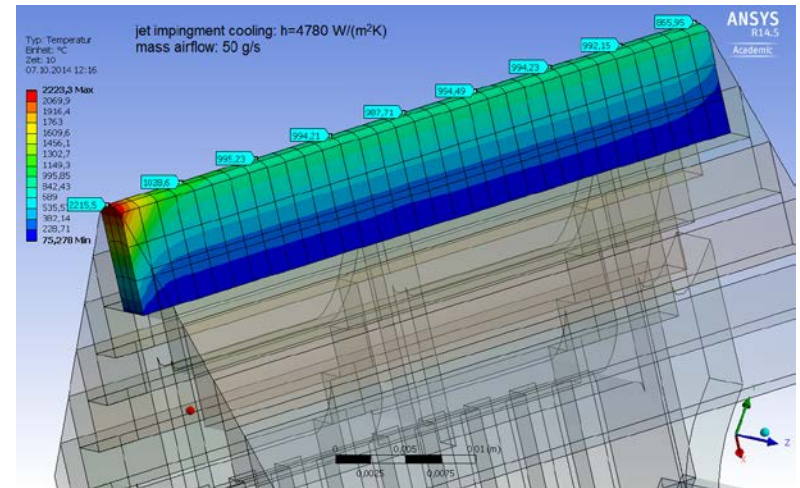
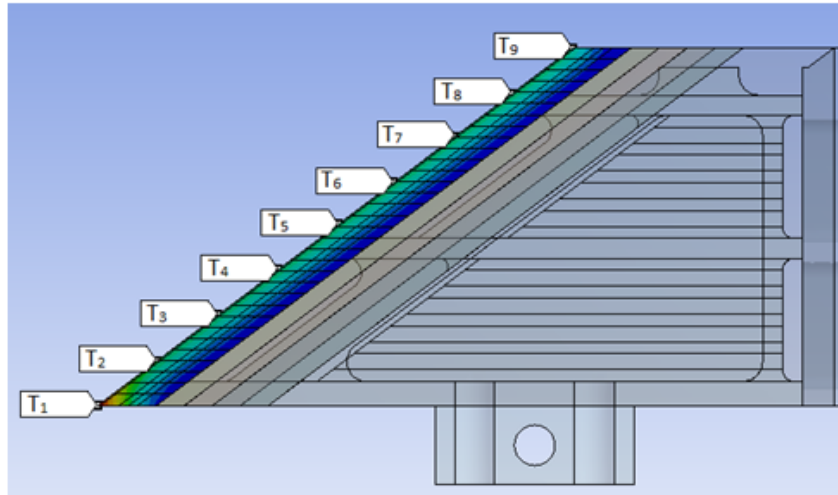
Testing in L3K DLR's arc heated facility:
calculation by Dr. B. Esser (DLR) for the radiused leading edge
of 0.8 mm for the two constant wall temperatures of 1000 K



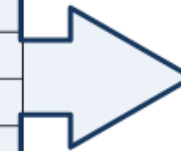
Temperature distribution on the leading edge:



Temperature distribution on the leading edge:

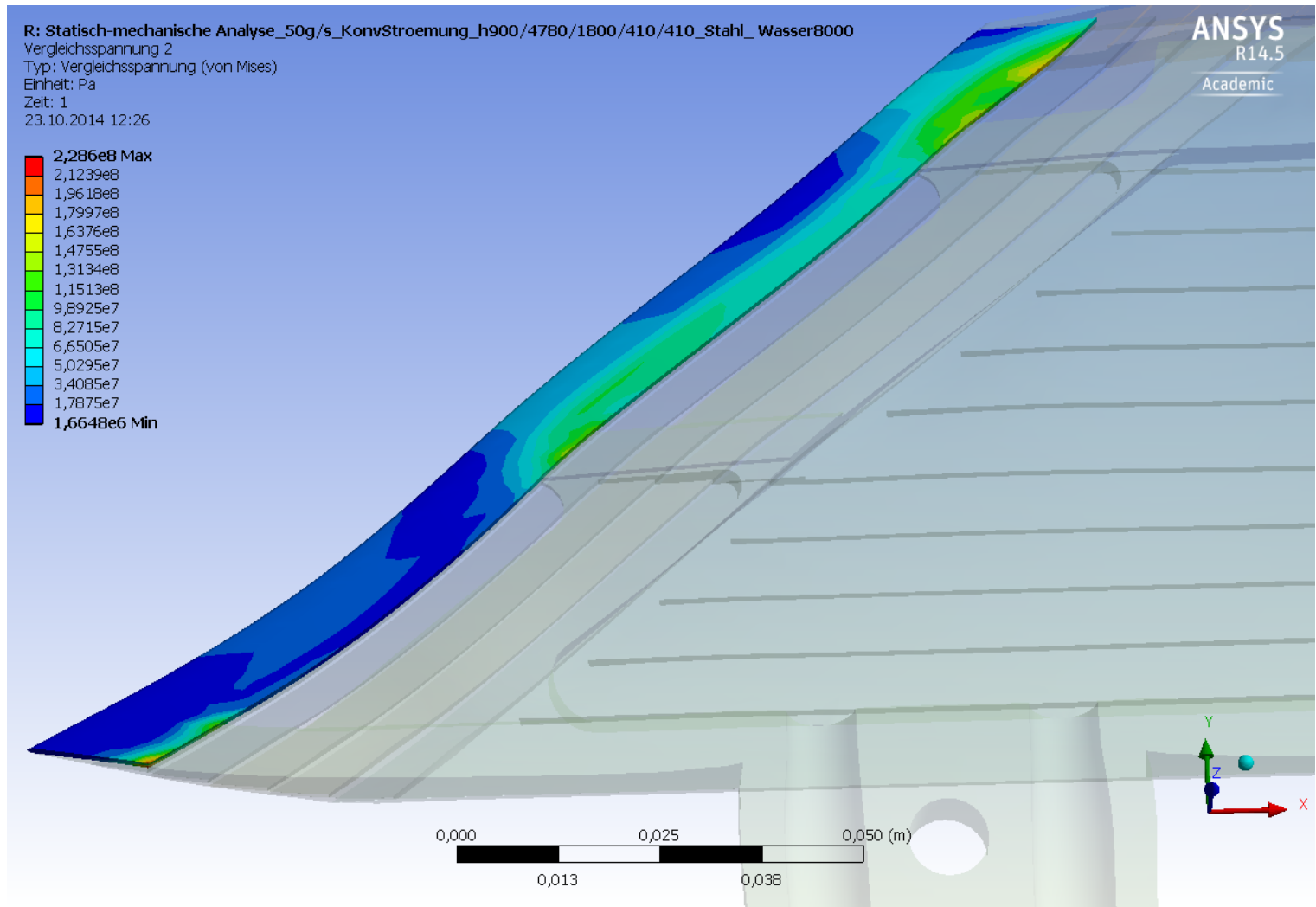


T, °C	25 g/s		50 g/s	
	h=2800 W/(m²K)	h=3000 W/(m²K)	h=4455 W/(m²K)	h=4780 W/(m²K)
T ₁	2303,9	2292,9	2226,5	2215,5
T ₂	1104,8	1093,4	1033,2	1028,6
T ₃	1068,1	1056,8	1003,9	995,23
T ₄	1065,5	1056,7	1003,1	994,21
T ₅	1055,3	1046,3	995,88	987,71
T ₆	1065,9	1053,8	1001,7	994,49
T ₇	1066,1	1056,6	1002,4	994,23
T ₈	1060,1	1050,7	999,62	992,15
T ₉	945,27	919,18	872,84	865,95



$T_{\max} < 1000 \text{ }^{\circ}\text{C}$

Equivalent Stress (von-Mises) in leading TMC layer



Task 3.1: Progress

- State:
 - Canard geometry and heat boundary conditions were set according to the data of the partners (TISICS, L3K DLR's arc heated facility team)
 - Model for the canard (CANARD Model (I)) has been set up
 - Numerical simulation indicated the high temperature levels which exceed the material's (titanium and TMCs) operational limits
 - Occurring slot velocities for impingement cooling were detected to be too low which effects in low heat transfer coefficients and hence cooling efficiency
 - Multiple options of the nozzle geometry were calculated in order to increase the impingement heat transfer coefficient
 - Primary variations allowed to increase the impingement coefficient up to ten times: from 148 up to 1500 W/(m²K)
 - As optimized option the cooling core geometrie with a thin slit nozzle was chosen. Further reduction in width of 0,5 mm led to almost double increase of cooling: 2800 W/(m²K)
 - Further variations (CANARD Model (II)) were conducted for the original and reduced slot lengths and for the nominal and doubled air mass flows of 25 and 50 g/s.

- D3.1.4 Results of “FEA of TMC ATLLAS generic leading edge model wing”
 - The maximum impingement cooling was achieved for the case with the reduced slot width of 0,5 mm and reduced slot length of ca 45 mm at the doubled air mass flow of 50 g/s: $h_{avg}=4780 \text{ W/(m}^2\text{K)}$
 - The maximum temperature of the leading TMC edge at the doubled air mass flow does not exceed of 1000 °C
 - The high temperature peaks at the bottom part of the leading edges of ~ 2200 °C were by numerical simulation obtained. Dr. Burkhard Esser suggests that it can be attributed to an artificial numerical effect based on a 2D external heat load as boundary conditions. Based on the results from Atlas-1, he does not expect significant increase in temperature

[1]. **Martin**, H. (1977). Heat and mass transfer between impinging gas jets and solid surfaces. Adv. Heat Transfer 13, 1–60.

Arroy of Slot Nozzle

Range of validity: $1500 < Re < 40000$, $0.008 \leq f \leq 2.5 f_0$, and $1 \leq H/S \leq 40$

Average Nusselt number Nu_{avg} :

$$Nu_{avg} = Pr^{0.42} \times 2/3 (f_0)^{3/4} (2 \times Re_B / (f/f_0 + f_0/f))^{2/3}$$

$$f_0 = [60 + 4(H/S - 2)^2]^{-1/2}$$

where S - twice slot width = nozzle hydraulic diameter
 f - relative nozzle area

Equations are for a developed jet.

[2]. Incropera, F., DeWitt, D.: Fundamentals of Heat and Mass Transfer, 2nd ed., Wiley & Sons, New York 1985

Force Turbulent Convection

Range of validity: $0.7 > Pr < 120$; $10000 < Re < 160000$; $L/D > 10$,

Average Nusselt number Nu_{avg} :

$$Nu_{avg, a, D} = 0.021 (Re_{a, D})^{0.8} (Pr_a)^{0.43} (Pr_a/Pr_w)^{0.25} \epsilon_l$$

where:

$Nu_{avg, a, D}$

average Nusselt number: $Nu = (h D)/k$

$Re_{a, D}$

Reynolds Number: $Re = (D V \rho)/\mu$

Pr_a, Pr_w

Prandtl Number: $Pr = (\mu C_p)/k$

ϵ_l

correlation coefficient: $\epsilon_l = 1.38 (L/D)^{-0.12}$

D characteristic length parameter (e.g. diameter for flow through a pipe or around a circular cylinder at $L/D > 10$, where L is length of pipe), m

k thermal conductivity of the fluid, W/(m K)

V characteristic velocity (e.g. average velocity for flow through a pipe or tube, m/s)

ρ density of the fluid, kg/m³

μ viscosity of the fluid, (Pa s)

C_p heat capacity of the fluid, (J/(kg K))

Index "a" denotes air as cooling fluid. All properties were taken for the air at the input temperature of 20 °C at 1 bar (s. Tab. 1) or at 4 bar (s. Tab. 2)

Index "w" refers to the air properties at the wall temperature (e.g. 800 °C).

Annex 3

Air properties used in the calculations:

Tab. 1: pressure = 1 bar and $T=20\text{ }^{\circ}\text{C}$:

Density, (kg/m^3)	1,189
Specific Heat Capacity, ($\text{J}/(\text{kg K})$)	1,0068
Thermal Conductivity, ($\text{W}/(\text{m K})$)	2,57E-02
Dynamic viscosity, (Pa s)	1,82E-05
Kinetic viscosity, (m^2/s)	1,53E-05
Prandtl number ($20\text{ }^{\circ}\text{C}$)	0,7153
Prandtl number ($800\text{ }^{\circ}\text{C}$)	0,734

Tab. 2: pressure = 4 bar and $T=20\text{ }^{\circ}\text{C}$:

Density, (kg/m^3)	4,771
Specific Heat Capacity, ($\text{J}/(\text{kg K})$)	1,012
Thermal Conductivity, ($\text{W}/(\text{m K})$)	2,58E-02
Dynamic viscosity, (Pa s)	1,83E-05
Kinetic viscosity, (m^2/s)	3,83E-06
Prandtl number ($20\text{ }^{\circ}\text{C}$)	0,716
Prandtl number ($800\text{ }^{\circ}\text{C}$)	0,734